

- ment applies unambiguously to both reversible and irreversible enzymes, and whether the 'efficiency function' these authors derive is in fact the relevant function that is optimized under evolutionary selection pressures. However, this seminal work is an important starting point for understanding the evolutionary rationale behind the internal thermodynamic properties of enzymes.
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PRO EXPERIMENTIS

Large scale preparation of oxidized streptolysin O using molecular filtration

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Summary. Oxidized streptolysin O, suitable for the determination of antistreptolysin O in whole blood, has been prepared from crude broth culture of *S. pyogenes* by molecular filtration using membranes with nominal mol. wt limit 10,000.

A new hemolytic method for the determination of antistreptolysin O (ASO) in whole blood has been proposed¹. The method is based on some characteristic properties of streptolysin O (SO): the oxidized form of the toxin can bind the specific antibodies but cannot interact with the red cell membrane. After addition of a reducing agent, both free and antibody-bound toxin interact with membrane receptors, but only the free toxin is able to cause red cell hemolysis. These principles form the basis of a new diagnostic method for the determination of ASO^{1,2}.

The oxidized SO was originally prepared from crude cultures of *Streptococcus pyogenes* by precipitation with ammonium sulfate, followed by centrifugation, dialysis and oxidation with hydrogen peroxide¹. The excess H₂O₂ was then removed by dialysis and the residual unoxidized SO was inactivated by addition of CuCl₂, followed by extensive dialysis. Although this method gave oxidized SO which could be used in the diagnostic test, the procedure proved to be time-consuming, and unsuitable for large-scale production.

In the present paper we report the results of experiments using molecular filtration for both concentration and purification of the initial crude broth culture and for dialysis after treatment with H₂O₂ and CuCl₂.

Crude broth cultures of *S. pyogenes* were prepared as previously described, with slight modifications. After 10 h growth, the bacteria were removed by filtration under pressure on Seitz filters type K7 and EKS, arranged in series. The titre of the toxin was determined measuring both the hemolytic units (HU) and the combining units (CU) as previously described¹.

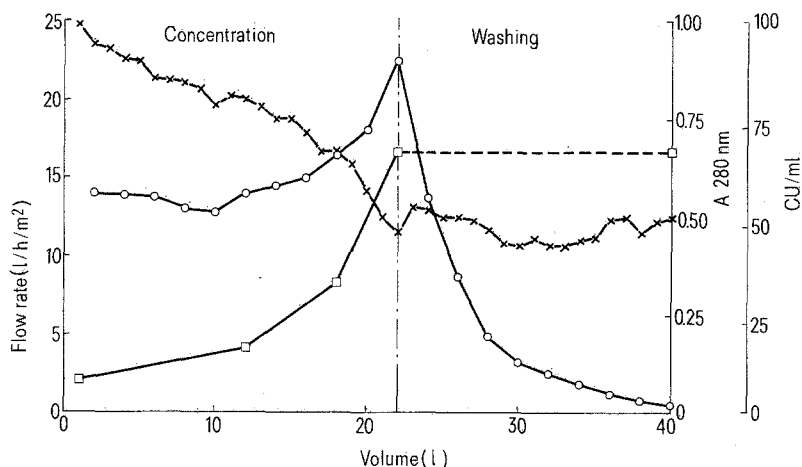
The concentration and purification of streptolysin by molecular filtration was performed with a 'high volume plastic cassette' assembled with PTGC membranes (nominal mol. wt limit=10,000) (Millipore, USA), fed by a piston pump generating a pressure of 4 at. The total filtering surface used was 0.92 m².

The figure shows the results of a typical experiment, performed on a 24-l batch of filtered crude broth culture. During the concentration phase, an increase was observed in the protein concentration in the filtrate, expressed as the absorbance at 280 nm, due to the presence of proteins partially retained by the membrane, which were removed only at a higher concentration. During the washing phase, keeping the retentate volume constant at 3 l, the protein concentration decreased rapidly. The washing was interrupted when the absorbance at 280 nm reached about 1, corresponding to removal of about 84% of the proteins.

Analytical characteristics of streptolysin O during the various phases of the preparation procedure

Solution	Volume (ml)	CU/ml	Protein* (mg/ml)	Specific activity (UE/mg protein)	Yield (%)
Initial broth culture	24,000	10	18.3	7	—
Concentrated and purified SO	2580	92	26.7	48	100
Oxidized SO	5450	41	8.9	72	94.1
Oxidized and CuCl ₂ -treated SO	6400	33	6.7	60	88.9

*Determined with the method of Lowry et al.⁵ using bovine serum albumin as standard.



Concentration and purification of a crude broth culture of *S. pyogenes* by molecular filtration. O, absorbance at 280 nm, after dilution 1:40; □, titre of the toxin (CU/ml); *, flow rate (l/h/m²).

The SO titre of the retentate increased during the concentration phase, then remained practically constant during the washing, with quantitative recovery. The filtrate flow decreased in the concentration phase, settling at values of about 10–12 l/h/m² during the washing.

The material was then subjected to treatment with H₂O₂ and with CuCl₂ as previously reported¹. Dialysis in tubes was, however, replaced by diafiltration; this was performed using the same system as that adopted for the initial concentration and purification phase. Removal of excess reagents (H₂O₂ or CuCl₂) required 5–6 volumes of water, with a flow of 14–15 l/h/m². Spot tests^{3,4} were used to monitor removal of H₂O₂ and Cu²⁺.

The table shows the analytical characteristics of SO during the various phases of the preparation procedure. The yield in CU was always approximately 90% in different experiments, with an average 8-fold increase in specific activity.

The SO obtained with the present method proved fully satisfactory for the determination of ASO titre in whole blood. The total time required for the experiment described above was about 12 h, including time for washings and general maintenance of the plant. The system is easy to operate, and being modular, its potentiality can be varied according to requirements.

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